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(54) **Film extruded from an in situ blend of ethylene copolymers**

Extrudierter Film aus in situ Mischungen von Aethylencopolymeren

Feuille extrudée à partir d'un mélange in situ de copolymères d'éthylène

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(56) References cited:  
**EP-A- 0 321 964 EP-A- 0 404 368**  
**US-A- 5 405 901**

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**EP 0 773 257 B1**

**Description****Technical Field**

5 [0001] This invention relates to shrink film extruded from a blend of ethylene copolymers prepared in a series of polymerization reactors.

**Background Information**

10 [0002] For many years, high pressure low density polyethylenes, which are highly branched polymers, were considered to be the resin of choice for commercial shrink film applications. The key property that facilitates the use of high pressure low density polyethylene for these applications is the long chain branching. The long chain branching makes possible the development of high melt stresses, which can be frozen into the film at the frost line during tubular film extrusion. In other words, sufficient strain hardening occurs during tubular film extrusion, for example, to generate in  
15 the film the frozen stresses that are required for shrink film applications. Under shrink tunnel conditions, the frozen-in stresses cause the film to shrink around the item to be packaged thus securing it firmly. These resins also have a relatively low stress relaxation rate, which facilitates a retention of the shrink forces needed to provide support for the packaged goods.

[0003] Unlike high pressure low density polyethylene, narrow molecular weight distribution linear low density polyethylene commonly used for tubular film extrusion has only short chain branching, the branches corresponding in length to the alpha-olefin that is copolymerized with ethylene to produce it. Without long chain branching, however, narrow molecular weight distribution linear low density polyethylene stresses relax too rapidly during melt extrusion to provide the high melt stresses, which can be frozen into the film. This is particularly true of the transverse direction of the narrow molecular weight distribution linear low density polyethylene film, which is stretched much less than the machine direction during film extrusion and, therefore, has virtually no shrinkage in that direction. As a result, narrow molecular weight distribution linear low density polyethylene is unacceptable for shrink film application because it sags around the material to be packaged instead of holding-it securely.

[0004] Manufacturers of linear low density polyethylene (LLDPE) were, therefore, seeking to identify an LLDPE, which was suitable for shrink film applications; was easier to process than the high pressure low density polyethylene resins; and, finally, would result in a film, which would outperform high pressure resin films in terms of those properties most desirable in shrink films. This was accomplished in United States Patent 4,814,135. In this patent, it was found that, in order to achieve a shrinkage of at least about 10 percent in the important transverse direction, a high weight average molecular weight of at least 250,000 together with a minor amount of a molecular weight species of at least about 500,000 was, among other defined parameters, necessary. It would be economically advantageous to be able  
35 to provide a shrink film having a transverse directional shrinkage of at least about 10 percent at a narrow blow up ratio, but at a much lower molecular weight, for the reason that extrusion processability is facilitated thereby.

**Disclosure of the Invention**

40 [0005] An object of this invention, therefore, is to provide a relatively low molecular weight shrink film having a transverse directional shrinkage of at least about 5 percent at a narrow blow up ratio. Other objects and advantages will become apparent hereinafter.

[0006] According to the present invention such shrink films have been discovered, the films being extruded from an in situ blend of polymers produced in two reactors connected in series. Steps and conditions, which can be used to provide the in situ blend, are described below.

45 [0007] The shrink film comprises a blend of copolymers of ethylene and one or more alpha-olefins having 3 to 12 carbon atoms formed in situ, said blend having a melt index in the range of about 0.2 to about 3.5 grams per 10 minutes, and preferably about 0.5 to about 3.5 grams per 10 minutes; a melt flow ratio in the range of about 50 to about 175; a molecular weight in the range of about 90,000 to about 225,000; a Mw/Mn ratio of at least about 8; and a density in  
50 the range of 0.910 to 0.940 gram per cubic centimeter, said shrink film being formed at a blow up ratio in the range of about 2:1 to about 6:1 and having the following properties:

- (i) at about 135 degrees C, a shrinkage of at least about 50 percent in the machine direction and zero or positive shrinkage in the transverse direction;
- 55 (ii) melt stress is zero or positive kilopascals; and
- (iii) a cooled stress of at least about  $0.35 \times 10^3$  kilopascals.

## Description of the Preferred Embodiment(s)

[0008] The gauge or thickness of the shrink film can be in the range of about 0.5 to about 6 mils, and is preferably in the range of about 1 to about 2.5 mils. The optimum gauge is about 1.2 mils.

[0009] The shrink films can be produced by various extrusion techniques such as blown film extrusion and slot cast biaxial orientation extrusion. Tubular film extrusion is preferred, particularly air cooled blown tubular film extrusion. Typical apparatus and a procedure for blown tubular film extrusion is described below. The minimum values for critical shrink film properties are as follows:

(i) Shrinkage at about 135°C. (approximate shrink tunnel temperature) in the machine direction is at least about 50 percent, and, in the transverse direction, zero or positive shrinkage and preferably zero to about 40 percent.

(ii) Shrink forces with the regard to melt stress is zero or positive kilopascals; preferably about 14 to about 103 kilopascals; and most preferably about 35 to about 69 kilopascals.

(iii) Cooled stress is at least about  $0.35 \times 10^3$  kilopascals and is preferably about  $0.85 \times 10^3$  to about  $2 \times 10^3$ . The only upper limits for these film properties are those that can be practically achieved.

[0010] The blend, which is used in the extruder, can be produced in two staged reactors connected in series wherein a mixture of resin and catalyst precursor is transferred from the first reactor to the second reactor in which another copolymer is prepared and blends in situ with the copolymer from the first reactor. The process is generally described, for example, in United States Patents 5,047,468 and 5,126,398; however, the conditions have to be adjusted to provide the desired properties in the in situ blend.

[0011] The copolymers produced in each of the reactors are copolymers of ethylene and at least one alpha-olefin comonomer. The relatively high molecular weight copolymer is produced in what is referred to as the high molecular weight reactor, and the relatively low molecular weight copolymer is produced in what is referred to as the low molecular weight reactor. The alpha-olefin comonomer(s), which can be present in both of the reactors can have 3 to 12 carbon atoms, and preferably have 3 to 8 carbon atoms. The alpha-olefins are exemplified by propylene, 1-butene, 1-hexene, 4-methyl-1-pentene, or 1-octene. Any of the aforementioned comonomers can be used in either reactor. Preferred comonomer combinations are 1-butene/1-butene; 1-butene/1-hexene; 1-hexene/1-butene; and 1-hexene/1-hexene combinations.

[0012] The magnesium/titanium based catalyst system, which can be used to make the in situ blend, can be exemplified by the catalyst system described in United States patent 4,302,565 although the precursor is preferably unsupported. Another preferred catalyst system is one where the precursor is formed by spray drying such as the system described in United States patent 5,290,745.

[0013] The electron donor, if used in the catalyst precursor, is an organic Lewis base, liquid at temperatures in the range of about 0°C to about 200° C, in which the magnesium and titanium compounds are soluble. The electron donor can be an alkyl ester of an aliphatic or aromatic carboxylic acid, an aliphatic ketone, an aliphatic amine, an aliphatic alcohol, an alkyl or cycloalkyl ether, or mixtures thereof, each electron donor having 2 to 20 carbon atoms. Among these electron donors, the preferred are alkyl and cycloalkyl ethers having 2 to 20 carbon atoms; dialkyl, diaryl, and alkylaryl ketones having 3 to 20 carbon atoms; and alkyl, alkoxy, and alkylalkoxy esters of alkyl and aryl carboxylic acids having 2 to 20 carbon atoms. The most preferred electron donor is tetrahydrofuran. Other examples of suitable electron donors are methyl formate, ethyl acetate, butyl acetate, ethyl ether, dioxane, di-n-propyl ether, dibutyl ether, ethyl formate, methyl acetate, ethyl anisate, ethylene carbonate, tetrahydropyran, and ethyl propionate.

[0014] While an excess of electron donor is used initially to provide the reaction product of titanium compound and electron donor, the reaction product finally contains about 1 to about 20 moles of electron donor per mole of titanium compound and preferably about 1 to about 10 moles of electron donor per mole of titanium compound.

[0015] An activator compound, which is generally used with any of the titanium based catalyst precursors, can have the formula  $AlR_aX_bH_c$  wherein each X is independently chlorine, bromine, iodine, or OR'; each R and R' is independently a saturated aliphatic hydrocarbon radical having 1 to 14 carbon atoms; b is 0 to 1.5; c is 0 or 1; and  $a+b+c=3$ . Preferred activators include alkylaluminum mono- and dichlorides wherein each alkyl radical has 1 to 6 carbon atoms and the trialkylaluminums. A particularly preferred activator is a mixture of diethylaluminum chloride and tri-n-hexylaluminum. About 0.10 to about 10 moles, and preferably about 0.15 to about 2.5 moles, of activator can be used per mole of electron donor. The molar ratio of activator to titanium can be in the range of about 1:1 to about 10:1 and is preferably in the range of about 2:1 to about 5:1.

[0016] The hydrocarbyl aluminum cocatalyst can be represented by the formula  $R_3Al$  or  $R_2AlX$  wherein each R is independently alkyl, cycloalkyl, aryl, or hydrogen; at least one R is hydrocarbyl; and two or three R radicals can be joined to form a heterocyclic structure. Each R, which is a hydrocarbyl radical, can have 1 to 20 carbon atoms, and preferably has 1 to 10 carbon atoms. X is a halogen, preferably chlorine, bromine, or iodine. Examples of hydrocarbyl aluminum compounds are as follows: triisobutylaluminum, tri-n-hexylaluminum, di-isobutyl-aluminum hydride, dihexy-

luminum dihydride, di-isobutyl-hexylaluminum, isobutyl dihexylaluminum, trimethylaluminum, triethylaluminum, tripropylaluminum, triisopropylaluminum, tri-n-butylaluminum, trioctylaluminum, tridecylaluminum, tridodecylaluminum, tribenzylaluminum, triphenylaluminum, trinaphthylaluminum, tritolylaluminum, dibutylaluminum chloride, diethylaluminum chloride, and ethylaluminum sesquichloride. The cocatalyst compounds can also serve as activators and modifiers.

[0017] As noted above, it is preferred not to use a support. However, in those cases where it is desired to support the precursor, silica is the preferred support. Other suitable supports are inorganic oxides such as aluminum phosphate, alumina, silica/alumina mixtures, silica modified with an organoaluminum compound such as triethylaluminum, and silica modified with diethyl zinc. A typical support is a solid, particulate, porous material essentially inert to the polymerization. It is used as a dry powder having an average particle size of about 10 to about 250 microns and preferably about 30 to about 100 microns; a surface area of at least 200 square meters per gram and preferably at least about 250 square meters per gram; and a pore size of at least about 100 angstroms and preferably at least about 200 angstroms. Generally, the amount of support used is that which will provide about 0.1 to about 1.0 millimole of titanium per gram of support and preferably about 0.4 to about 0.9 millimole of titanium per gram of support. Impregnation of the above mentioned catalyst precursor into a silica support can be accomplished by mixing the precursor and silica gel in the electron donor solvent or other solvent followed by solvent removal under reduced pressure. When a support is not desired, the catalyst precursor can be used in liquid form.

[0018] Activators can be added to the precursor either before and/or during polymerization. In one procedure, the precursor is fully activated before polymerization. In another procedure, the precursor is partially activated before polymerization, and activation is completed in the reactor. Where a modifier is used instead of an activator, the modifiers are usually dissolved in an organic solvent such as isopentane and, where a support is used, impregnated into the support following impregnation of the titanium compound or complex, after which the supported catalyst precursor is dried. Otherwise, the modifier solution is added by itself directly to the reactor. Modifiers are similar in chemical structure and function to the activators. For variations, see, for example, United States patent 5,106,926. The cocatalyst is preferably added separately neat or as a solution in an inert solvent, such as isopentane, to the polymerization reactor at the same time as the flow of ethylene is initiated.

[0019] United States patent 5,106,926 provides another example of a magnesium/titanium based catalyst system comprising:

- (i) a catalyst precursor having the formula  $Mg_dTi(OR)_eX_f(ED)_g$  wherein R is an aliphatic or aromatic hydrocarbon radical having 1 to 14 carbon atoms or COR' wherein R' is a aliphatic or aromatic hydrocarbon radical having 1 to 14 carbon atoms; each OR group is the same or different; X is independently chlorine, bromine or iodine; ED is an electron donor; d is 0.5 to 56; e is 0, 1, or 2; f is 2 to 116; and g is  $1.5d+2$ ;
  - (ii) at least one modifier having the formula  $BX_3$  or  $AlR_{(3-e)}X_e$  wherein each R is alkyl or aryl and is the same or different, and X and e are as defined above for component (a)
- wherein components (a) and (b) are impregnated into an inorganic support; and
- (iii) a hydrocarbyl aluminum cocatalyst.

[0020] The precursor is prepared from a titanium compound, a magnesium compound, and an electron donor. Titanium compounds, which are useful in preparing these precursors, have the formula  $Ti(OR)_eX_h$  wherein R, X, and e are as defined above for component (a); h is an integer from 1 to 4; and e+h is 3 or 4. Examples of titanium compounds are  $TiCl_3$ ,  $TiCl_4$ ,  $Ti(OC_2H_5)_2Br_2$ ,  $Ti(OC_6H_5)_3Cl_3$ ,  $Ti(OCOCH_3)_3Cl_3$ , and  $Ti(OCOC_6H_5)_3Cl_3$ . The magnesium compounds include magnesium halides such as  $MgCl_2$ ,  $MgBr_2$ , and  $MgI_2$ . Anhydrous  $MgCl_2$  is a preferred compound. About 0.5 to 56, and preferably about 1 to 10, moles of the magnesium compounds are used per mole of titanium compounds.

[0021] The electron donor, the support, and the cocatalyst are the same as those described above. As noted, the modifier can be similar in chemical structure to the aluminum containing activators. The modifier has the formula  $BX_3$  or  $AlR_{(3-e)}X_e$  wherein each R is independently alkyl having 1 to 14 carbon atoms; each X is independently chlorine, bromine, or iodine; and e is 1 or 2. One or more modifiers can be used. Preferred modifiers include alkylaluminum mono- and dichlorides wherein each alkyl radical has 1 to 6 carbon atoms; boron trichloride; and the trialkylaluminums. About 0.1 to about 10 moles, and preferably about 0.2 to about 2.5 moles, of modifier can be used per mole of electron donor. The molar ratio of modifier to titanium can be in the range of about 1:1 to about 10:1 and is preferably in the range of about 2:1 to about 5:1.

[0022] The entire catalyst system, which includes the precursor or activated precursor and the cocatalyst, is added to the first reactor. The catalyst is admixed with the copolymer produced in the first reactor, and the mixture is transferred to the second reactor. Insofar as the catalyst is concerned, only cocatalyst is added to the second reactor from an outside source.

[0023] The polymerization in each reactor is, preferably, conducted in the gas phase using a continuous fluidized process. A typical fluidized bed reactor is described in United States patent 4,482,687.

[0024] A relatively low melt index (or high molecular weight) copolymer is preferably prepared in the first reactor, and the relatively high melt index (or low molecular weight) copolymer is prepared in the second reactor. This can be referred to as the forward mode. Alternatively, the relatively low molecular weight copolymer can be prepared in the first reactor and the relatively high molecular weight copolymer can be prepared in the second reactor. This can be referred to as the reverse mode.

[0025] The first reactor is generally smaller in size than the second reactor because only a portion of the final product is made in the first reactor. The mixture of polymer and an active catalyst is usually transferred from the first reactor to the second reactor via an interconnecting device using nitrogen or second reactor recycle gas as a transfer medium.

[0026] In the high molecular weight reactor:

Because of the low values, instead of melt index, flow index is determined and those values are used in this specification. The flow index can be in the range of about 0.01 to about 30 grams per 10 minutes, and is preferably in the range of about 0.2 to about 6 grams per 10 minutes. The molecular weight of this polymer is, generally, in the range of about 400,000 to about 480,000. The density of the copolymer can be 0.860 to 0.940 gram per cubic centimeter, and is preferably in the range of 0.900 to 0.930 gram per cubic centimeter. The melt flow ratio of the polymer can be in the range of about 20 to about 70, and is preferably about 22 to about 45.

[0027] In the low molecular weight reactor:

A relatively high melt index (or low molecular weight) copolymer is prepared in this reactor. The high melt index can be in the range of about 50 to about 3000 grams per 10 minutes, and is preferably in the range of about 100 to about 1500 grams per 10 minutes. The molecular weight of the high melt index copolymer is, generally, in the range of about 14,000 to about 30,000. The density of the copolymer prepared in this reactor can be 0.900 to 0.970 gram per cubic centimeter, and is preferably in the range of 0.905 to 0.945 gram per cubic centimeter. The melt flow ratio of this copolymer can be in the range of about 20 to about 70, and is preferably about 20 to about 45.

[0028] The blend or final product, as removed from the second reactor, can have a melt index in the range of about 0.2 to about 3.5 grams per 10 minutes, and preferably has a melt index in the range of about 0.5 to about 3.5 grams per 10 minutes. The melt flow ratio can be in the range of about 50 to about 175. The molecular weight of the final product can be in the range of about 90,000 to about 225,000, and is preferably in the range of about 120,000 to about 200,000. The density of the blend can be in the range of 0.910 to 0.940 gram per cubic centimeter, and is preferably in the range of 0.918 to 0.926 gram per cubic centimeter.

[0029] It will be understood that generally the in situ blend can be characterized as a multimodal resin, usually bimodal or trimodal. In some cases, however, the two components making up the blend are sufficiently close in average molecular weight that there is no discernible discontinuity in the molecular weight curve.

[0030] The properties of these resins are strongly dependent on the proportion of the high molecular weight component, i.e., the low melt index component. For a staged reactor system, the proportion of the high molecular weight component is controlled via the relative production rate in each reactor. The relative production rate in each reactor can, in turn, be controlled by a computer application program, which monitors the production rate in the reactors (measured by heat balance) and then manipulates the ethylene partial pressure in each reactor and catalyst feed rate in order to meet the production rate, the production rate split, and catalyst productivity requirements. The broad molecular weight distribution is reflected in an Mw/Mn ratio of at least about 8, and is preferably at least about 10. The only upper limit is the bounds of practicality. Mw is the weight average molecular weight; Mn is the number average molecular weight; and the Mw/Mn ratio can be referred to as the polydispersity index, which is a measure of the breadth of the molecular weight distribution.

[0031] The weight ratio of copolymer prepared in the high molecular weight reactor to copolymer prepared in the low molecular weight reactor can be in the range of about 0.5:1 to about 2:1.

[0032] The catalyst system, ethylene, alpha-olefin, and hydrogen are continuously fed into the first reactor; the polymer/catalyst mixture is continuously transferred from the first reactor to the second reactor; ethylene, alpha-olefin, and hydrogen, as well as cocatalyst are continuously fed to the second reactor. The final product is continuously removed from the second reactor.

[0033] In the low melt index, as reflected in flow index, reactor:

The mole ratio of alpha-olefin to ethylene can be in the range of about 0.05:1 to about 0.4:1, and is preferably in the range of about 0.09:1 to about 0.26:1. The mole ratio of hydrogen (if used) to ethylene can be in the range of about 0.0001:1 to about 0.3:1, and is preferably in the range of about 0.001:1 to about 0.18:1. The operating temperature is generally in the range of about 60° C to about 100° C. Preferred operating temperatures vary depending on the density desired, i.e., lower temperatures for lower densities and higher temperatures for higher densities.

[0034] In the high melt index reactor:

The mole ratio of alpha-olefin to ethylene can be in the range of about 0.1:1 to about 0.6:1, and is preferably in the range of about 0.2:1 to about 0.45:1. The mole ratio of hydrogen to ethylene can be in the range of about 1:1 to about 3:1, and is preferably in the range of about 1.6:1 to about 2.2:1. The operating temperature is generally in the range of about 70° C to about 100° C. As mentioned above, the temperature is preferably varied with the desired density.

[0035] The pressure is generally the same in both the first and second reactors. The pressure can be in the range of about 200 to about 450 psi and is preferably in the range of about 280 to about 350 psig. A typical fluidized bed reactor can be described as follows:

The bed is usually made up of the same granular resin that is to be produced in the reactor. Thus, during the course of the polymerization, the bed comprises formed polymer particles, growing polymer particles, and catalyst particles fluidized by polymerization and modifying gaseous components introduced at a flow rate or velocity sufficient to cause the particles to separate and act as a fluid. The fluidizing gas is made up of the initial feed, make-up feed, and cycle (recycle) gas, i.e., comonomers and, if desired, modifiers and/or an inert carrier gas.

[0036] The essential parts of the reaction system are the vessel, the bed, the gas distribution plate, inlet and outlet piping, a compressor, cycle gas cooler, and a product discharge system. In the vessel, above the bed, there is a velocity reduction zone, and, in the bed, a reaction zone. Both are above the gas distribution plate.

[0037] A typical and preferred catalyst system is one where the precursor is formed by spray drying and is used in slurry form. Such a catalyst precursor, for example, contains titanium, magnesium, and an electron donor, and, optionally, an aluminum halide. The precursor is then introduced into a hydrocarbon medium such as mineral oil to provide the slurry form. See United States patent 5,290,745.

[0038] The in situ polyethylene blend can be produced using the following **typical** procedure:

Ethylene is copolymerized with 1-hexene and 1-butene. Trimethylaluminum (TMA) cocatalyst is added to each reactor during polymerization. The pressure in each reactor is 300 psia. Each polymerization is continuously conducted after equilibrium is reached.

[0039] Polymerization is initiated in the first reactor by continuously feeding the above catalyst precursor and cocatalyst, TMA, into a fluidized bed of polyethylene granules together with ethylene, 1-hexene, and hydrogen. The TMA is first dissolved in isopentane (5 percent by weight TMA). The resulting copolymer mixed with active catalyst is withdrawn from the first reactor and transferred to the second reactor using nitrogen as a transfer medium. The second reactor also contains a fluidized bed of polyethylene granules. Ethylene, 1-butene, and hydrogen are introduced into the second reactor where they come into contact with the copolymer and catalyst from the first reactor. Additional cocatalyst is also introduced. The product blend is continuously removed.

[0040] A **typical** procedure for preparing shrink film by blown tubular film extrusion is as follows: The extruder is equipped with a fluted mixing screw capable of providing the level of melt homogeneity that is found in current commercial tubular film extrusions. 3 inch and 6 inch bottom fed, spiral mandrel tubular film dies, each equipped with a 0.04 inch die pin, are used to extrude the polymer or copolymer. The size of the die orifice is maintained at 0.036 inch. The films are extruded at an 8 pound/hour/inch of die circumference die rate using a blow-up ratio (BUR) ranging (in the present invention) from about 2:1 to about 6:1, and preferably about 2.5:1 to about 4.5:1; melt temperatures in the range of about 175°C to about 210°C; and a frost line height of 12 inches.

[0041] Variations of these extrusion conditions to optimize film properties for specific applications can be made by anyone having ordinary skill in the art of shrink film extrusion.

[0042] The extruder can be, for example, a 1.5 or 3.5 inch extruder having a 3 inch (75 millimeter) die and a 40 mil (1.0 millimeter) gap. The thickness of the film provided and tested is 25 microns except in examples 1, 2 and 3 where it is 35, 50, and 65, respectively. The temperatures are as follows: barrel profile=190°C; adapter=200°C; die=210°C; and melt=250°C. The screw speed is 120 revolutions per minute (rpm); the melt pressure is 158 bars; the extrusion rate is 22 kilograms per hour; and the drive current is 10 amperes.

[0043] Terms and properties mentioned are defined or determined as follows:

[0044] Machine direction is the direction in which the film web is pulled from the die of the film extruder.

[0045] Transverse direction is the direction of the web, which is perpendicular to the machine direction and parallel to the web.

[0046] Shrinkage (the percent change in film dimension) is determined as follows:

$$\text{Machine direction shrinkage (percent)} = \frac{\text{LiMD} - \text{LsMD}}{\text{LiMD}} \times 100$$

$$\text{Transverse direction shrinkage (percent)} = \frac{\text{LiTD} - \text{LsTD}}{\text{LiTD}} \times 100$$

wherein

LiMD = initial machine direction length

LsMD = machine direction length after shrinkage

LiTD = initial transverse direction length

LsTD = transverse direction length after shrinkage.

[0047] Another way to determine shrinkage is as follows:

A 3 inch x 3 inch film specimen is cut so that the MD and TD directions are parallel to the sides of the specimen. The specimen is placed in a circulating oil bath at 124°C. for 60 seconds using a suitable holder such that the film can shrink freely, but not curl. The specimen is removed from the bath and quenched briefly in water. The MD and TD shrinkage is obtained by measuring the specimen in the MD and TD direction and making the following calculation:

$$\text{Percent Shrinkage} = \frac{\text{Initial Width minus Final Width}}{\text{Initial Width}} \times 100$$

[0048] Melt stresses are stresses frozen into the film at the frost line. Cooled stresses are crystalline stresses remaining in the solidified film. Melt stress and cooled stress are determined as follows: A film specimen one inch wide is clamped in a set of "Instron" jaws so that they are six inches apart. With the "Instron" jaws stationary, a 500-watt radiant heater is swung in at a given distance from the film causing the film to melt and start to shrink. The stress in the melt state is recorded as a load on the "Instron" chart. As the melt stress begins to decay, the heater is removed and the film is allowed to cool. MD and TD directions. The values are given in kilopascals (KPa).

[0049] Melt strength is the resistance to deformation in the melt. It can be defined as that property which resists thinning and subsequent hole formation (burnthrough) when subjected to the shrink stresses released while the film is in the molten state in the oil bath at an elevated temperature (usually 124°C.). Then, the time for the film to pull apart under the weight attached is recorded as the melt strength in seconds. For example, for a four mil sample, an 18 gram weight is usually used which gives a stress of 8.3 psi in oil. Failure time is usually between 10 to 70 seconds. Temperatures and weights are varied according to film thickness and melting point.

[0050] Melt Flow is determined under ASTM D-1238-79 in grams per 10 minutes. It is similar to melt index. Melt index is determined under ASTM D-1238, Condition E. It is measured at 190°C and 2.16 kilograms. and reported as grams per 10 minutes. Flow index is determined under ASTM D-1238, Condition F. It is measured at 190°C and 10 times the weight used in determining melt index, and reported as grams per 10 minutes. Melt flow ratio is the ratio of flow index to melt index.

[0051] Density is determined under ASTM D-1505. A plaque is made in accordance with ASTM D-1928, Procedure C, and conditioned for one hour at 100°C to approach equilibrium crystallinity. Measurement for density is then made in a density gradient column and density values are reported in kilogram per cubic meter.

[0052] Film gauge is the thickness of the film. The value can be given in microns or mils.

[0053] Blow-up ratio is the ratio of die diameter to bubble diameter. The bubble diameter is determined as follows:  $2 \times \text{layflat} / \pi$ . The "layflat" refers to the width of a flattened bubble.

[0054] Molecular weight distribution is determined via Size Exclusion Chromatography using a Waters™ 150C with trichlorobenzene as solvent at 140 degrees C with a broad molecular weight distribution standard and broad molecular weight distribution calibration method.

[0055] Die rate is defined as pounds per hour per inch of die circumference.

[0056] Frost line height is that distance off of the base of the die during which the polymer undergoes a phase transformation from a viscous liquid to a solid.

[0057] Conventional additives, which can be introduced into the blend, are exemplified by antioxidants, ultraviolet absorbers, antistatic agents, pigments, dyes, nucleating agents, fillers, slip agents, fire retardants, plasticizers, processing aids, lubricants, stabilizers, smoke inhibitors, viscosity control agents, and crosslinking agents, catalysts, and boosters, tackifiers, and anti-blocking agents. Aside from the fillers, the additives can be present in the blend in amounts of about 0.1 to about 10 parts by weight of additive for each 100 parts by weight of polymer blend. Fillers can be added in amounts up to 200 parts by weight and more for each 100 parts by weight of the blend. The additives can be added to the reactor(s) or extruder via a suitable medium such as a conventional hydrocarbon diluent.

[0058] Further, the blend can be, in turn, blended with other polyethylenes, such as high pressure low density polyethylenes (HP-LDPE), for use in shrink films in varying amounts depending on the properties desired. The melt index of the HP-LDPE can be in the range suitable for blown films and slot cast films, preferably about 0.15 to about 6 grams per 10 minutes.

[0059] The shrink film of the invention, in addition to having the frozen stresses so important in shrink film applications, has the following advantages:

- (i) the excellent shrink properties of in situ blends, particularly those containing significant amounts of 1-butene and/or 1-hexene;
- (ii) the blends can be extruded on a standard LLDPE line or a conventional high pressure (HP) LDPE line employing narrow die gaps, e.g., 35 mils, and at normal blow-up ratios, e.g., 2:1 to 4:1; and
- (iii) there is an economic advantage through film down-gauging compared to shrink film made with HP-LDPE blends or HP-LDPE/LLDPE blends. This economic advantage is captured in the shrink film market by capitalizing on the

inherent film toughness characterized by films extruded from an in situ blend of ethylene copolymers.

[0060] Patents mentioned in this specification are incorporated by reference herein.

[0061] The invention is illustrated by the following examples.

## Examples

[0062] Two in situ blend resins are prepared, i.e., Resin A and Resin B. The reaction conditions for the preparation of Resin A are set forth in Table I and the reaction conditions for the preparation of Resin B are set forth in Table II. Resin A is prepared in the reverse mode. Resin B is prepared in the standard mode.

[0063] In the reverse mode, the low molecular weight copolymer is prepared in the first reactor; transferred together with active catalyst to the second reactor; and blended in situ with the high molecular weight copolymer, which is prepared in the second reactor. In the standard mode, the high molecular weight copolymer is prepared in the first reactor; transferred together with active catalyst to the second reactor; and blended in situ with the low molecular weight copolymer, which is prepared in the second reactor.

[0064] The catalyst precursor is formed by spray drying and is used in slurry form. It contains titanium, magnesium, and aluminum halides, and an electron donor, and is attached to the surface of silica. The precursor is then introduced into a hydrocarbon medium such as mineral oil to provide the slurry form. See United States patent 5,290,745 ('745). The catalyst precursor and method of preparing same used in the examples is the same composition and preparation method as example 1 of '745. For low density operation, such as that described herein, a reduced catalyst precursor is used. Typically, the molar ratio of diethylaluminum chloride (DEAC) to tetrahydrofuran (THF) is 0.45 and the molar ratio of tri-n-hexylaluminum to tetrahydrofuran is 0.20. The addition of diethylaluminum chloride and tri-n-hexylaluminum (TnHAL) is achieved by an in-line reduction system in which the diethylaluminum chloride and tri-n-hexylaluminum are fed to the reactor concurrently with the catalyst precursor in order to produce a reduced catalyst.

[0065] Ethylene is copolymerized with a comonomer in each of two fluidized bed reactors. Each polymerization is continuously conducted after equilibrium is reached under conditions set forth in the Tables.

[0066] Polymerization is initiated in the first reactor by continuously feeding the above catalyst precursor and cocatalyst, trimethylaluminum (TMA), into a fluidized bed of polyethylene granules together with ethylene, a comonomer, and hydrogen. The cocatalyst is first dissolved in isopentane (5 percent by weight cocatalyst). Higher concentrations of cocatalyst in solution can also be used as well as using the cocatalyst neat. The resulting copolymer mixed with active catalyst is withdrawn from the first reactor and transferred to the second reactor using either nitrogen or second reactor cycle gas as a transfer medium. The second reactor also contains a fluidized bed of polyethylene granules. Again, ethylene, a comonomer, and hydrogen are introduced into the second reactor where the gases come into contact with the copolymer and catalyst from the first reactor. Additional cocatalyst is also introduced. The product blend is continuously removed.

[0067] Resin A has a melt index of 0.7 gram per 10 minutes; a flow index of 68.0 grams per 10 minutes; a melt flow ratio of 98.0; and a density of 0.923 gram per cubic centimeter. Resin B has a melt index of 0.7 gram per 10 minutes; a flow index of 69.0 grams per 10 minutes; a melt flow ratio of 98.0; and a density of 0.922 gram per cubic centimeter.

[0068] Resin C is a high pressure low density polyethylene (HP-LDPE). It is a homopolymer of ethylene prepared by a conventional high pressure process. Resin C has a melt index of 2 grams per 10 minutes; a flow index of 120 grams per 10 minutes; a melt flow ratio of 60; and a density of 0.920 gram per cubic centimeter. Resin D is also an HP-LDPE, and is a homopolymer of ethylene prepared by a conventional high pressure process. Resin D has a melt index of 0.9 gram per 10 minutes; a flow index of 73 grams per 10 minutes; a melt flow ratio of 80; and a density of 0.920 gram per cubic centimeter.

[0069] In addition to polymerization conditions for Resin A in Table I and Resin B in Table II, film extrusion conditions and film properties are given in Tables III and IV.

[0070] The equipment for extruding the blends into film in Table III is a 40 millimeter (1 1/2 inches) Old Sterling™ extruder having a Barrier™ screw; a 50 millimeter (2 inch) die; and a 1 millimeter (40 mil) die gap. The screw rpm is a variable.

[0071] The equipment for extruding the blends into film in Table IV is a 90 millimeter (3 1/2 inches) Gloucester™ extruder having a DSB II screw; a 150 millimeter (6 inch) die; and a 0.9 millimeter (35 mil) die gap. The die rate is 10 pounds per hour per inch.

Table I

reaction conditions	reactor I	reactor II
temperature (° C)	85	72



Table I (continued)

reaction conditions	reactor I	reactor II
pressure (psia)	298	251
C2 partial pressure (psia)	66.7	53
H2/C2 molar ratio	1.96	0.018
C4/C2 molar ratio	0.28	0
C6/C2 molar ratio	0	0.166
C2 feed (lbs/hr)	15250	10639
H2 feed (lbs/hr)	19.3	0.065
C4 feed (lbs/hr)	1186	0
C6 feed (lbs/hr)	0	2964
cocatalyst	10% TMA	10% TMA
catalyst feed rate (lbs/hr)	8.87	
production rate (lbs/hr)	16072	12725
total production rate (lbs/hr)	----	28797
ethylene split	0.589	0.411
titanium split	0.591	0.409
fluidized bulk density (lbs/cu ft)	15.54	14.4
bed weight (lbs)	62210	60225
bed level (ft)	39.3	37.2
bed volume (cu ft)	4003	4182
residence time (hrs)	3.871	2.091
STY (lbs/hr/cu ft)	4.01	3.04

Table II

reaction conditions	reactor I	reactor II
temperature (° C)	70	85
pressure (psia)	305	306
C2 partial pressure (psia)	23.5	84.8
H2/C2 molar ratio	0.057	1.79
C4/C2 molar ratio	0	0.23
C6/C2 molar ratio	0.147	0.006
C2 feed (lbs/hr)	12816	15492
H2 feed (lbs/hr)	0.25	59
C4 feed (lbs/hr)	0	1606
C6 feed (lbs/hr)	2037	0
cocatalyst	10% TMA	10% TMA
cocatalyst feed rate (lbs/hr)	36	13
hexane feed rate (lbs/hr)	540	0
catalyst feed rate (lbs/hr)	19.6	----
production rate (lbs/hr)	14600	16300
total production rate (lbs/hr)	----	30900
ethylene split	0.453	0.547
titanium split	0.490	0.50
SGV (ft/sec)	2.07	2.2
fluidized bulk density (lbs/cu ft)	12.42	16.98
bed weight (lbs)	52161	72962
bed level (ft)	39.1	39.7
bed volume (cu ft)	4200	4297
residence time (hrs)	3.573	2.361

Table II (continued)

reaction conditions	reactor I	reactor II
% condensing (wt)	4.4	0
STY (lbs/hr/cu ft)	3.48	3.79

TABLE III

TABLE III						
example	RESIN	BUR	GAUGE (MILS)	DIE RATE LBS/ HR/IN	LBS/HR	
1	C	3:1	1.5	7.3	46	
2	C	3:1	2	11.9	75	
3	A	3.5:1	1.5	7.6	48	
4	A	4:1	1.5	9.4	59	
5	A	4:1	2	9.4	59	
6	A	4:1	2.5	9.4	59	
example	RESIN	MD SHRINK (%)	TD SHRINK (%)	MD HOT STRESS (PSI)	MD COLD STRESS (PSI)	
1	C	85	23	19.4	258.9	
2	C	80	25	11.8	208.3	
3	A	80	10	6	272.8	
4	A	77	17	4.9	241.3	
5	A	73	17	4.8	232.2	
6	A	70	20	3.6	246	
Extrusions Conditions:						
example	1	2	3	4	5	6
resin	C	C	A	A	A	A
gauge (mils)	1.5	2	1.5	1.5	2	2.5
(mm)	(.04)	(.05)	(.04)	(.04)	(.05)	(.06)
BUR	3:1	3:1	3.5:1	4:1	4.0:1	4.0:1
Screw rpm	90	154	120	152	152	152
Melt Temp (°C)	199	204	210	216	216	216
Head Pressure	1200	1300	2000	2300	2300	2300
(psi)						
(MPa)	(8.3)	(9.0)	(13.8)	(15.9)	(15.9)	(15.9)
Amps	7.0	8.5	10	11	11.0	11.0
Die Rate						
(lbs/hr/in)	7.3	11.9	7.6	9.4	9.4	9.4
(kg/hr/cm)	(1.3)	(2.1)	(1.4)	(1.7)	(1.7)	(1.7)
Specific Output Rate						
(lbs/hr/rpm)	0.51	0.49	0.4	0.39	0.39	0.39
(kg/hr/rpm)	(0.23)	(0.22)	(0.18)	(0.18)	(.18)	.18)

Table IV

			Resin B		Resin D	
5	MI (g/10 min)		0.7		0.9	
	HLMI (g/10 min)		69.0		73	
	MFR		98.0		80.0	
10	Density (g/cc)		0.922		0.920	
Extrusion Conditions:						
15	Melt Temperature (°C)		218		207	
	Head Pressure psi		3900		2900	
	(Mpa)		(26.9)		(20.0)	
20	Amps		110		90	
	Die Rate		10.0		10.3	
	lbs/hr/in (kg/hr/cm)		(1.8)		(1.8)	
25	Specific Output Rate		3.8		4.3	
	lbs/hr/rpm (kg/hr/rpm)		(1.7)		(2.0)	
30	Bubble Stability		GOOD		GOOD	
	Melt Fracture		NONE		NONE	
35	Film Properties: : 1.25 mil film (30 micron), 2.5:1 BUR					
	Tensile Strength	MD	5000	(34.5)	3400	(23.4)
	psi (MPa)	TD	3600	(24.8)	2700	(18.6)
40	Elongation at break	MD	560		260	
	(%)	TD	800		540	
	Secant Modulus	MD	36500	(255)	27400	(186)
45	(psi) (MPa)	TD	42700	(296)	33400	(228)
	Elmendorf Tear	MD	133	(51.2)	198	(77.0)
	grams/mil (N/mm)	TD	1000	(385)	163	(62.8)
50	Shrinkage	MD	76%		78%	
	(%)	TD	0%		20%	
	Hot Melt Stress	MD	3.3	(22.8)	4.5	(31.0)
	(psi)(kPa)					
55	Cold Stress	MD	124	(855)	236	(1627)
	(psi)(kPa)					

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Table IV (continued)

		Resin B		Resin D		
5	Film Properties : 1.25 mil film (30 micron), 2.5:1 BUR					
	Puncture energy/mil (J/ mm)		20.0	(89)	14.7	(65.4)
	Dart Drop (g)		150		97	
	Haze (%)		35.0		5.0	
	Gloss (45 deg.)		18.0		68.0	
15   <						

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Table IV (continued)

		Resin B		Resin D	
Film Properties : 1.25 mil film (30 micron), 3.0:1 BUR					
5	Hot Melt Stress (psi)(kPa)	MD	2.6 (17.9)	4.8 (33.1)	
	Cold Stress (psi)(kPa)	MD	138 (952)	195 (1345)	
10	Puncture energy/mil (J/mm)		19.0 (84.6)	16.7 (74.3)	
	Dart Drop (g)		125	103	
15	Haze(%)		32.0	4.6	
	Gloss (45 deg.)		20.0	72.0	
Film Properties : 2.25 mil film (55 micron), 3.0:1 BUR					
20	Tensile Strength psi (MPa)	MD	4400 (30.3)	3800 (26.2)	
	Elongation at break (%)	TD	4100 (28.3)	3200 (22.1)	
	Secant Modulus (psi) (MPa)	MD	800	430	
25	Elmendorf Tear grams/mil (N/mm)	TD	900 (248)	600 (193)	
	Shrinkage (%)	MD	36000 (262)	27600 (193)	
	Hot Melt Stress (psi)(kPa)	TD	38000 (94.3)	27600 (43.9)	
30	Cold Stress (psi)(kPa)	MD	245 (192.5)	114 (55.8)	
	Puncture energy/mil (J/mm)	TD	500	145	
	Dart Drop (g)	MD	63%	70%	
	Haze (%)	TD	16%	40%	
35	Gloss (45 deg.)	MD	2.0 (13.8)	2.0 (13.8)	
	Hot Melt Stress (psi)(kPa)	MD	191 (1317)	69 (478)	
	Cold Stress (psi)(kPa)	MD	18.0 (80.1)	16.5 (73.4)	
40	Puncture energy/mil (J/mm)				
	Dart Drop (g)		260	191	
	Haze (%)		33.0	4.2	
	Gloss (45 deg.)		22.0	79.0	
45	Film Properties: 1.25 mil film (30 micron), 3.5:1 BUR				
	Tensile Strength psi (MPa)	MD	4600 (31.7)	3300 (22.8)	
50	Elongation at break (%)	TD	3200 (22.1)	3300 (22.8)	
	Secant Modulus (psi) (MPa)	MD	600	300	
	Elmendorf Tear grams/mil (N/mm)	TD	700 (255)	500 (172)	
55	Shrinkage (%)	MD	37000 (283)	25000 (206)	
	Hot Melt Stress (psi)(kPa)	TD	41000 (82.8)	29600 (28.9)	
	Cold Stress (psi)(kPa)	MD	215	75	
	Puncture energy/mil (J/mm)				
	Dart Drop (g)				
	Haze (%)				
	Gloss (45 deg.)				

Table IV (continued)

		Resin B		Resin D	
Film Properties: 1.25 mil film (30 micron), 3.5:1 BUR					
grams/mil (N/mm)	TD	840	(327)	175	(67.4)
Shrinkage (%)	MD	75%		77%	
	TD	20%		50%	
Hot Melt Stress (psi)(kPa)	MD	2.1	(14.5)	3.8	(26.2)
Cold Stress (psi)(kPa)	MD	53	(365)	135	(931)
Puncture energy/mil (J/mm)		17.0	(75.7)	17.0	(75.7)
Dart Drop (g)		150		127	
Haze (%)		32.0		4.5	
Gloss (45 deg.)		20.0		72.0	
Film Properties: 2.25 mil film (55 micron), 3.5:1 BUR					
Tensile Strength	MD	4400	(30.3)	3000	(20.7)
psi (MPa)	TD	3800	(26.2)	2800	(19.3)
Elongation at break (%)	MD	875		480	
	TD	900		580	
Secant Modulus (psi) (MPa)	MD	37900	(261)	26000	(179)
	TD	40700	(281)	27000	(186)
Elmendorf Tear	MD	275	(105.8)	73	(28.1)
grams/mil (N/mm)	TD	425	(163.6)	125	(48.1)
Shrinkage (%)	MD	60%		70%	
	TD	30%		45%	
Hot Melt Stress (psi)(kPa)	MD	2.0	(13.8)	7.3	(50.3)
Cold Stress (psi)(kPa)	MD	180	(1241)	216	(1489)
Puncture energy/mil (J/mm)		16.0	(71.2)	16.0	(71.2)
Dart Drop (g)		300		185	
Haze (%)		33.0		4.8	
Gloss (45 deg.)		22.0		79.0	
Notes to Examples:					
1. MI = melt index					
2. HLMI = flow index					
3. MFR = melt flow ratio					
4. Bubble stability is determined by the speed of the line. The faster the speed (prior to failure) the better the bubble stability.					
5. Dart impact (dart drop) is determined under ASTM D-1709, methods A and B. It is given in grams.					
6. Elmendorf Tear is determined under ASTM D-1992. It is given in grams per mil.					

Table IV (continued)

	Resin B	Resin D
Film Properties:		
5	2.25 mil film (55 micron), 3.5:1 BUR	
	7. MD = machine direction 8. TD = transverse direction 9. Tensile Strength is measured in accordance with ASTM D-882. 10. Elongation is measured in accordance with ASTM D-882. 10 11. Tensile strength at yield point is measured in accordance with ASTM D-882. 12. Secant Modulus is measured in accordance with ASTM D-882. 13. Haze is determined under ASTM D- 1003. 14. Gloss is determined under ASTM D- 2457. 15. Melt fracture is determined by visually examining the film. 15 Each film is given a value from 1 to 9 with the value 1 being the worst case of melt fracture and the value 9 representing essentially no melt fracture as follows: 1 = severely gross 1 = severely gross 20 2 = gross 3 = gross shark skin 4 = severe shark skin 5 = shark skin 6 = rough surface 25 7 = slightly rough surface 8 = minor imperfection, but acceptable 9 = essentially no melt fracture 16. Puncture resistance: the test is carried out with a metal cylinder, open at both ends, having a diameter of 75 millimeters and a length of 100 millimeters. One open end is covered with the sample film, which is held taut by a metal band surrounding that end of the cylinder (similar to a drum). The cylinder is placed in a vertical position with the film covered end up. Then, the film is pressed with the sharp point of a nail-like rod (5 millimeters in diameter and 150 millimeters in length) and a force is exerted against the film. When the film is broken, the force exerted is measured in grams. 30 17. STY (lbs/hr/cu ft) is the space time yield defined as the pounds per hour of polymer produced per cubic foot of fluidized bed. 35	

#### Claims

- 40 1. A shrink film comprising a blend of copolymers of ethylene and one or more alpha-olefins having 3 to 12 carbon atoms formed in situ, said blend having a melt index in the range of from 0.2 to 3.5 grams per 10 minutes; a melt flow ratio in the range of from 50 to 175; a molecular weight in the range of from 90,000 to 225,000; a Mw/Mn ratio of at least about 8; and a density in the range of from 0.910 to 0.940 gram per cubic centimeter, the shrink film being formed at a blow up ratio in the range of from 2:1 to 6:1 and having the following properties:
  - 45 (i) at about 135 degrees C, a shrinkage of at least about 50 percent in the machine direction and zero or positive shrinkage in the transverse direction;
  - (ii) melt stress is zero or positive kilopascals; and
  - 50 (iii) a cooled stress of at least about  $0.35 \times 10^3$  kilopascals.
2. A film as claimed in claim 1 wherein the molecular weight of the blend is in the range of from 120,000 to 225,000.
3. A film as claimed in claim 1 or claim 2 wherein the blend of copolymers is formed in a high molecular weight reactor and a low molecular weight reactor, the polymer formed in the high molecular weight reactor having a flow index
  - 55 in the range of from 0.2 to 6 grams per 10 minutes and a density in the range of from 0.900 to 0.930 gram per cubic centimeter and the polymer formed in the low molecular weight reactor having a melt index in the range of from 100 to 1500 grams per 10 minutes and a density in the range of from 0.905 to 0.945 gram per cubic centimeter.

4. A film as claimed in any one of the preceding claims wherein the blend has a melt index in the range of from 0.5 to 3.5 grams per 10 minutes.

5. A film as claimed in any one of the preceding claims wherein the blend has an Mw/Mn ratio of at least about 10.

6. A shrink film comprising a blend of copolymers of ethylene and one or more alpha-olefins having 3 to 8 carbon atoms formed in situ, said blend having a melt index in the range of from 0.5 to 3.5 grams per 10 minutes; a melt flow ratio in the range of from 50 to 175; a molecular weight in the range of from 130,000 to 200,000; a Mn/Mw ratio of at least about 10; and a density in the range of from 0.918 to 0.926 gram per cubic centimeter, the shrink film being formed at a blow up ratio in the range of from 2:1 to 4.5:1 and having the following properties:

(i) at about 135 degrees C, a shrinkage of at least about 60 percent in the machine direction and of zero to 40 percent in the transverse direction;

(ii) melt stress of from 14 to 103 kilopascals; and

(iii) a cooled stress of from  $0.85 \times 10^3$  to  $2 \times 10^3$  kilopascals,

said film having been extruded to a gauge in the range of from 25 to 87.5 micrometres (1 to 3.5 mils) and having been produced in situ by contacting ethylene and at least one alpha-olefin comonomer having 3 to 8 carbon atoms with a magnesium/titanium based catalyst system in each of two reactors connected in series, under polymerization conditions, wherein (a) the polymer formed in the high molecular weight reactor has a flow index in the range of from 0.2 to 1 gram per 10 minutes and a density in the range of from 0.900 to 0.930 gram per cubic centimeter and (b) the polymer formed in the low molecular weight reactor has a melt index in the range of from 100 to 1500 grams per 10 minutes and a density in the range of from 0.905 to 0.945 gram per cubic centimeter, the weight ratio of high molecular weight reactor polymer to the low molecular weight reactor polymer being in the range of from 0.5:1 to 2:1.

7. A film as claimed in claim 6 wherein the blend is produced under the following conditions:

(i) in the high molecular weight reactor: the mole ratio of comonomer(s) to ethylene is in the range of from 0.05:1 to 0.4:1 and the mole ratio of hydrogen, if used, to ethylene is in the range of from 0.0001:1 to 0.3:1; and

(ii) in the low molecular weight reactor: the mole ratio of comonomer(s) to ethylene is in the range of from 0.1:1 to 0.6:1 and the mole ratio of hydrogen to ethylene is in the range of from 1:1 to 2.5:1.

## Patentansprüche

1. Schrumpffolie umfassend eine Mischung von Copolymeren aus Ethylen und einem oder mehreren alpha-Olefinen mit mindestens 3 bis 12 Kohlenstoffatomen, gebildet *in situ*, wobei die Mischung einen Schmelzindex im Bereich von 0,2 bis 3,5 g pro zehn Minuten; ein Schmelzflussverhältnis im Bereich von 50 bis 175; ein Molekulargewicht im Bereich von 90.000 bis 225.000; ein Mw/Mn-Verhältnis von mindestens etwa 8; und eine Dichte im Bereich von 0,910 bis 0,940 g/cm<sup>3</sup> aufweist, wobei die Schrumpffolie bei einem Aufblasverhältnis im Bereich von 2:1 bis 6:1 gebildet wird und die folgenden Eigenschaften aufweist:

(i) bei etwa 135° C eine Schrumpfung von mindestens etwa 50 Prozent in der Maschinenrichtung und Null oder positive Schrumpfung in der Querrichtung;

(ii) die Schmelzspannung beträgt Null oder positive Kilopascal; und

(iii) eine Kaltspannung von mindestens etwa  $0,35 \times 10^3$  Kilopascal.

2. Folie nach Anspruch 1, wobei das Molekulargewicht der Mischung im Bereich von 120.000 bis 225.000 ist.

3. Folie nach Anspruch 1 oder 2, wobei die Mischung aus Copolymeren in einem Hochmolekulargewicht-Reaktor und einem Niedrigmolekulargewicht-Reaktor gebildet wird, wobei das in dem Hochmolekulargewicht-Reaktor gebildete Polymer einen Fließexponenten im Bereich von 0,2 bis 6 g pro zehn Minuten und eine Dichte im Bereich von 0,900 bis 0,930 g/cm<sup>3</sup> und das in dem Niedrigmolekulargewicht-Reaktor gebildete Polymer einen Schmelzindex im Bereich von 100 bis 1.500 g pro zehn Minuten und eine Dichte im Bereich von 0,905 bis 0,945 g/cm<sup>3</sup> aufweist.



4. Folie nach einem der vorangehenden Ansprüche, wobei die Mischung einen Schmelzindex im Bereich von 0,5 bis 3,5 g pro 10 Minuten aufweist.

5. Folie nach einem der vorangehenden Ansprüche, wobei die Mischung ein Mw/Mn-Verhältnis von mindestens etwa 10 aufweist.

6. Schrumpffolie umfassend eine Mischung aus Copolymeren aus Ethylen und einem oder mehreren alpha-Olefinen mit drei bis acht Kohlenstoffatomen, gebildet *in situ*, wobei die Mischung einen Schmelzindex im Bereich von 0,5 bis 3,5 g pro zehn Minuten; ein Schmelzflussverhältnis im Bereich von 50 bis 175; ein Molekulargewicht im Bereich von 130.000 bis 200.000; ein Mn/Mw-Verhältnis von mindestens etwa 10; und eine Dichte im Bereich von 0,918 bis 0,926 g/cm<sup>3</sup> aufweist, wobei die Schrumpffolie bei einem Aufblasverhältnis im Bereich von 2:1 bis 4,5:1 gebildet wird und die folgenden Eigenschaften aufweist:

(i) bei etwa 135° C eine Schrumpfung von mindestens etwa 60 % in der Maschinenrichtung und von Null bis 40 % in der Querrichtung;

(ii) Schmelzspannung von 14 bis 103 Kilopascal; und

(iii) eine Kaltspannung von  $0,85 \times 10^3$  bis  $2 \times 10^3$  Kilopascal,

wobei die Folie auf ein Foliendickenmaß im Bereich von 25 bis 87,5 Mikrometer (1 bis 3,5 mls) extrudiert worden und *in situ* hergestellt worden ist durch Inkontaktbringen von Ethylen und mindestens einem alpha-Olefin-Comonomer mit 3 bis 8 Kohlenstoffatomen mit einem Katalysatorsystem auf Magnesium/Titan-Basis in einem jeden von zwei in Serie verbundenen Reaktoren unter Polymerisationsbedingungen, wobei (a) das in dem Hochmolekulargewicht-Reaktor gebildete Polymer einen Fließexponenten im Bereich von 0,2 bis 1 g pro zehn Minuten und eine Dichte im Bereich von 0,900 bis 0,930 g/cm<sup>3</sup> aufweist und (b) das in dem Niedrigmolekulargewicht-Reaktor gebildete Polymer einen Schmelzindex im Bereich von 100 bis 1.500 g pro zehn Minuten und eine Dichte im Bereich von 0,905 bis 0,945 g/cm<sup>3</sup> aufweist, wobei das Gewichtsverhältnis von Hochmolekulargewicht-Reaktor-Polymer zu Niedrigmolekulargewicht-Reaktor-Polymer im Bereich von 0,5:1 bis 2:1 ist.

7. Folie nach Anspruch 6, wobei die Mischung unter den folgenden Bedingungen hergestellt wird:

(i) im Hochmolekulargewicht-Reaktor: das Molverhältnis von Comonomer(en) zu Ethylen ist im Bereich von 0,05:1 bis 0,4:1 und das Molverhältnis von Wasserstoff, falls verwendet, zu Ethylen ist im Bereich von 0,0001:1 bis 0,3:1; und

(ii) im Niedrigmolekulargewicht-Reaktor: das Molverhältnis von Comonomer(en) zu Ethylen ist im Bereich von 0,1:1 bis 0,6:1 und das Molverhältnis von Wasserstoff zu Ethylen ist im Bereich von 1:1 bis 2,5:1.

## Revendications

1. Feuille rétractable comprenant un mélange de copolymères d'éthylène et d'une ou plusieurs alpha-oléfinen comprenant de 3 à 12 atomes de carbone formé *in situ*, ledit mélange présentant un indice de viscosité à chaud compris dans la gamme allant de 0,2 à 3,5 grammes par 10 minutes; un taux d'écoulement à chaud compris dans la gamme allant de 50 à 175; un poids moléculaire compris dans la gamme allant de 90 000 à 225 000; un rapport Mw/Mn d'au moins environ 8; et une masse volumique comprise dans la gamme allant de 0,910 à 0,940 gramme par centimètre cube, la feuille rétractable étant formée à un taux de soufflage compris dans la gamme allant de 2/1 à 6/1 et ayant les propriétés suivantes:

(i) à environ 135 degrés C, un retrait d'au moins environ 50 pour cent dans le sens machine et un retrait nul ou positif dans le sens transversal;

(ii) une contrainte à chaud égale à zéro kilopascal ou positive; et

(iii) une contrainte à l'état refroidi d'au moins environ  $0,35 \times 10^3$  kilopascals.

2. Feuille selon la revendication 1, dans laquelle le poids moléculaire du mélange est compris dans la gamme allant de 120 000 à 225 000.

3. Feuille selon la revendication 1 ou la revendication 2, dans laquelle le mélange de copolymères est formé dans un réacteur pour haut poids moléculaire et dans un réacteur pour bas poids moléculaire, le polymère formé dans le réacteur pour haut poids moléculaire présentant un indice d'écoulement compris dans la gamme allant de 0,2 à 6 grammes par 10 minutes et une masse volumique comprise dans la gamme allant de 0,900 à 0,930 gramme par centimètre cube, et le polymère formé dans le réacteur pour bas poids moléculaire présentant un indice de viscosité à chaud compris dans la gamme allant de 100 à 1 500 grammes par 10 minutes et une masse volumique comprise dans la gamme allant de 0,905 à 0,945 gramme par centimètre cube.

4. Feuille selon l'une quelconque des revendications précédentes, dans laquelle le mélange présente un indice de viscosité à chaud compris dans la gamme allant de 0,5 à 3,5 grammes par 10 minutes.

5. Feuille selon l'une quelconque des revendications précédentes, dans laquelle le mélange présente un rapport Mw/Mn d'au moins environ 10.

6. Feuille rétractable comprenant un mélange de copolymères d'éthylène et d'une ou plusieurs alpha-oléfines comprenant de 3 à 8 atomes de carbone formé in situ, ledit mélange présentant un indice de viscosité à chaud compris dans la gamme allant de 0,5 à 3,5 grammes par 10 minutes ; un taux d'écoulement à chaud compris dans la gamme allant de 50 à 175 ; un poids moléculaire compris dans la gamme allant de 130 000 à 200 000 ; un rapport Mw/Mn d'au moins environ 10 ; et une masse volumique comprise dans la gamme allant de 0,918 à 0,926 gramme par centimètre cube, la feuille rétractable étant formée à un taux de soufflage compris dans la gamme allant de 2/1 à 4,5/1 et ayant les propriétés suivantes :

(i) à environ 135 degrés C, un retrait d'au moins environ 60 pour cent dans le sens machine et un retrait de zéro à 40 pour cent dans le sens transversal ;

(ii) une contrainte à chaud comprise entre 14 et 103 kilopascals ; et

(iii) une contrainte à l'état refroidi comprise entre  $0,85 \times 10^3$  et  $2 \times 10^3$  kilopascals,

ladite feuille ayant été extrudée à une épaisseur comprise dans la gamme allant de 25 à 87,5 micromètres (1 à 3,5 mils) et ayant été produite in situ par la mise en contact d'éthylène avec au moins un comonomère alpha-oléfine comprenant de 3 à 8 atomes de carbone avec un système de catalyseur à base de magnésium/titane dans chacun de deux réacteurs reliés en série, dans des conditions de polymérisation, où (a) le polymère formé dans le réacteur pour haut poids moléculaire présente un indice d'écoulement compris dans la gamme allant de 0,2 à 1 gramme par 10 minutes et une masse volumique comprise dans la gamme allant de 0,900 à 0,930 gramme par centimètre cube, et (b) le polymère formé dans le réacteur pour bas poids moléculaire présente un indice de viscosité à chaud compris dans la gamme allant de 100 à 1 500 grammes par 10 minutes et une masse volumique comprise dans la gamme allant de 0,905 et 0,945 gramme par centimètre cube, le rapport pondéral du polymère du réacteur pour haut poids moléculaire au polymère du réacteur pour bas poids moléculaire étant compris dans la gamme allant de 0,5/1 à 2/1.

7. Feuille selon la revendication 6, dans laquelle le mélange est produit dans les conditions suivantes :

(i) dans le réacteur pour haut poids moléculaire : le rapport molaire du (des) co-monomère(s) à l'éthylène est compris dans la gamme allant de 0,05/1 à 0,4/1, et le rapport molaire de l'hydrogène, si on en utilise, à l'éthylène est compris dans la gamme allant de 0,0001/1 à 0/3/1 ; et

(ii) dans le réacteur pour bas poids moléculaire : le rapport molaire du (des) co-monomère(s) à l'éthylène est compris dans la gamme allant de 0,1/1 à 0,6/1, et le rapport molaire de l'hydrogène à l'éthylène est compris dans la gamme allant de 1/1 à 2,5/1.

(19)



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**(54) Film extruded from an in situ blend of ethylene copolymers**

(57) A shrink film comprising a blend of copolymers of ethylene and one or more alpha-olefins having 3 to 12 carbon atoms formed in situ, said blend having a melt index in the range of from 0.2 to 3.5 grams per 10 minutes; a melt flow ratio in the range of from 50 to 175; a molecular weight in the range of from 90,000 to 225,000; a Mw/Mn ratio of at least about 8; and a density in the range of from 0.910 to 0.940 gram per cubic centimeter,

the shrink film being formed at a blow up ratio in the range of from 2:1 to 6:1 and having the following properties:

- (i) at about 135 degrees C, a shrinkage of at least about 50 percent in the machine direction and zero or positive shrinkage in the transverse direction;
- (ii) melt stress is zero or positive kilopascals; and
- (iii) a cooled stress of at least about  $0.35 \times 10^3$  kilopascals.

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# EUROPEAN SEARCH REPORT

Application Number  
EP 96 30 8064

DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int.Cl.6)
Y	EP 0 404 368 A (UNIPLAST IND INC) 27 December 1990 * page 2, line 31 - page 4, line 25 *	1-7	C08L23/08 C08J5/18
Y	US 5 405 901 A (DANIELL PAUL T ET AL) 11 April 1995 * column 3, line 3 - column 12, line 8 *	1-7	
D,A	EP 0 321 964 A (UNION CARBIDE CORP) 28 June 1989 * table 1 *	1-7	
			TECHNICAL FIELDS SEARCHED (Int.Cl.6)
			C08J C08L
The present search report has been drawn up for all claims			
Place of search <b>THE HAGUE</b>		Date of completion of the search <b>17 December 1998</b>	Examiner <b>Schmidt, H</b>
CATEGORY OF CITED DOCUMENTS		T : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons A : technological background O : non-written disclosure P : intermediate document	
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17-12-1998

Patent document cited in search report		Publication date	Patent family member(s)		Publication date
EP 0404368	A	27-12-1990	PT	94246 A	08-02-1991
US 5405901	A	11-04-1995	AU	678658 B	05-06-1997
			AU	1148495 A	18-01-1996
			BR	9500391 A	18-06-1996
			CA	2141474 A	07-01-1996
			EP	0691353 A	10-01-1996
			JP	8027205 A	30-01-1996
EP 0321964	A	28-06-1989	US	4814135 A	21-03-1989
			CA	1308858 A	13-10-1992
			CN	1035078 A,B	30-08-1989
			DE	3876082 A	24-12-1992
			GR	3007029 T	30-07-1993
			JP	1259923 A	17-10-1989
			JP	1932375 C	26-05-1995
			JP	6061813 B	17-08-1994
			KR	9310553 B	28-10-1993

EPO FORM P4459

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